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<p>(54) Title: METHOD OF PREPARING MICROPARTICLES OF PHYTOSTEROLS OR PHYTOSTANOLS</p> <p>(57) Abstract</p> <p>A method of preparing microparticles of one or more phytosterols, phytostanols or mixtures of both comprises: dispersing or suspending the phytosterols or phytostanols or mixtures of both in a semi-fluid, fluid or viscous vehicle; and exposing the vehicle so formed to impact forces.</p>		

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**Title:** METHOD OF PREPARING MICROPARTICLES OF PHYTOSTEROLS OR PHYTOSTANOLS

### **Field of the Invention**

The present invention relates to the field of phytosterol and phytostanol solutions, emulsions, dispersions and compositions and to the use of the foregoing in foods, beverages, pharmaceuticals and nutraceuticals.

### **Background of the Invention**

Phytosterols have received a great deal of attention due to their ability to decrease serum cholesterol levels when fed to a number of mammalian species, including humans. While the precise mechanism of action remains largely unknown, the relationship between cholesterol and phytosterols is apparently due, in part, to the similarities between the respective chemical structures (the differences occurring on the side chains of the molecules). It is assumed that phytosterol replaces cholesterol from the micellar phase thereby reducing its absorption.

Given that phytosterol in various combinations have been proven to have wide clinical and dietary applications in lowering total and low density lipoprotein cholesterol, the key problem now facing researchers in this field is the adaptation of the phytosterols and their hydrogenated counterparts, phytostanols for incorporation into delivery systems and the possible modification of phytosterols/stanols to enhance their efficacy. Studies have investigated how the form (for example crystalline, suspension, granular) in which the phytosterols are dosed impacts on their ability to lower serum cholesterol levels. Phytosterols are highly lipophilic, do not dissolve to any extent in the micellar phase in the digestive tract and are therefore not efficient at blocking cholesterol absorption. Oils and fats to a limited degree are capable of dissolving free phytosterols. Since only solubilized phytosterols inhibit the absorption of cholesterol, this "delivery" problem must be adequately addressed.

Early research focussed on grinding or dry milling the phytosterols in order to try and enhance solubility (US Patent Nos: 3,881,005 and 4,195,084 both to Eli Lilly). In addition, researchers have looked to the esterification of phytosterols in order to enhance solubility in delivery systems. German Patent 2035069/January 29, 1971 (analogous to US Patent No.3,751,569) describes the addition of phytosterol fatty acid esters to cooking oil. The significant drawback to this process, among others, is the use of non-food grade catalysts and reagents.

Similarly, the incorporation of phytosterols into delivery vehicles, whether they be food or pharmaceutical-based, for administration to humans has been fraught with difficulties. US Patent No. 4,588,717 to David E. Mitchell Medical Research Institute discloses a vitamin supplement with fatty acid esters of phytosterols. US Patent No. 5,270,041 to Marigen S.A. teaches the use of phytosterols, their esters and glucosides for the treatment of tumours. The preparation of this composition involves the use of hazardous chemical reagents which effectively precludes the phytosterol component's ready use in all but a limited pharmaceutical area.

In view of the high dietary and pharmaceutical usefulness of phytosterols, it would be advantageous to have a simple, safe and effective means to incorporate these sterols into delivery vehicles, including foods, beverages, nutraceuticals and pharmaceuticals. It is an object of the present invention to obviate or mitigate the above disadvantages.

### **Summary of the Invention**

The present invention provides, in a first part, a method of preparing microparticles of one or more phytosterols, phytostanols or mixtures of both which comprises dispersing or suspending the phytosterols and/or phytostanols in a semi-

fluid, fluid or viscous vehicle and then exposing the vehicle so formed to impact forces to produce microparticles.

The present invention also provides, in a second part, a method of incorporating one or more phytosterols, phytostanols or mixture of both into a delivery vehicle which comprises simultaneously introducing into a microfluidizer the phytosterols and/or stanols and the chosen delivery vehicle and operating the microfluidizer under suitable pressure.

The present invention further provides, in a third part, a composition comprising microparticles of one or more phytosterols, phytostanols or mixtures of both in a semi-fluid, fluid or viscous vehicle.

The present invention further provides foods, beverages, pharmaceuticals and nutraceuticals which comprise microparticles of phytosterols and/or phytostanols.

In addition, the present invention provides for the use of the compositions described herein to prevent or treat primary or secondary dyslipidemias and atherosclerosis including coronary heart disease, peripheral vascular disease and strokes in humans and animals.

What this method of reducing phytosterols and/or stanols into substantially uniform submicron particles achieves is two-fold. Firstly, the efficacy of the phytosterols/stanols in preventing and treating primary and secondary dyslipidemias and cardiovascular disease and in lowering serum cholesterol is enhanced by virtue of the more discrete particle size. Secondly, the ultimate dispersion or incorporation of the phytosterols/stanols into a delivery vehicle of choice is more uniform than has heretofore been achieved. There are many delivery vehicles into which the phytosterols/stanols may be incorporated in accordance with the methods of the present invention described below. Without limiting the generality of the foregoing, these

delivery vehicles may include any edible oil or aqueous food, beverage, nutraceutical or pharmaceutical matrix.

### **Preferred Embodiments of the Invention**

In essence, the method of preparing microparticles of phytosterols and/or phytostanols using impact forces in accordance with the present invention produces uniform submicron particles which are highly suitable for therapeutic and dietary uses as is or, alternatively, they may be incorporated into other food, beverage, nutraceutical or pharmaceutical-based delivery systems. It has been found that the phytosterols/stanols so prepared have greater solubility, not only in oil-based delivery systems but in other media and aqueous systems which opens the door for a vast array of options for their administration, particularly in the area of foods and beverages.

### **Impact Forces/Preparing Microparticles**

Prior researchers have attempted to reduce the particle size of phytosterols/phytostanols (hereinafter collectively referred to as "phytosterols" unless otherwise indicated) by conventional grinding and milling. These techniques are cumbersome, expensive and, because dry milling generates high energy, the produced particles could form aggregates. In addition, producing uniform particle size distribution below 10um is difficult if not impossible using these conventional techniques. In contrast, the "impact" forces described and claimed within the scope of the present invention allow for the production of smaller and more uniform particle size, with all of the attendant advantages. In addition, these "impact forces" result in faster processing times, higher reproducibility from batch to batch and allows for the production of more uniform dispersions and emulsions.

A preferred means to reduce the particle size of the phytosterols is by shear forces, wherein the semi-fluid, fluid or viscous vehicle comprising the dispersed or

suspended phytosterols is forced through an air-atomization or pneumatic nozzle or a microfluidizer. Particle size reduction may also be achieved by steep shearing gradients in high-speed stirrers or colloid mills.

Microparticles of phytosterols having a wide range of shapes and sizes may be prepared in accordance with the present invention. Depending on the type of impact force used, slightly different end products may be achieved. For example, when using an air-atomization nozzle, the air pressure and configuration of the nozzle effects the final microparticle size. Nonetheless, as used herein, the term microparticle shall refer to a solid particle typically ranging from about 1 to 1000 microns. Microparticles below 20 microns are most preferred for incorporation into foods, beverages and nutraceuticals. Although spherical particles are preferred for some applications (and are normally produced by air-atomization), it has been found that irregularly shaped microparticles of phytosterols are equally suitable for the ultimate incorporation into delivery vehicles.

The process of reducing phytosterol particle size in accordance with the present invention comprises the steps of:

- a) dispersing or otherwise suspending the phytosterol in a suitable semi-fluid, fluid or viscous vehicle; and then
- b) exposing the vehicle so formed to impact forces to produce microparticles.

These impact forces are preferably created by high-shear using either an air-atomization nozzle, a pneumatic nozzle, a high shear mixer or colloid mill or in a microfluidizer. In a most preferred form of the present invention, the impact forces are created using a microfluidizer.

#### **1) Microfluidization**

Microfluidization, or particle collision technology, achieves what traditional homogenizers, grinding mills and other equipment have failed adequately to do: create uniform dispersions, emulsions and the like comprising microparticulate phytosterols.

By way of comparison, traditional grinding mills have extensive limitations including contamination of products, scalability and control difficulties, extensive processing times and high support requirements. The alternative, homogenizer valves, which push fluids through a variable geometry spring-loaded valve, are also fraught with limitations including the requirement for a high volume through-put and low pressures (leading to variable particle size in end product).

In contrast, using particle collision technology as the "impact" force, the resultant particle size is smaller and more consistent due to the higher pressure attained in the microfluidization chamber (up to 40,000 psi compared to 10,000-12,000 in a standard homogenizer).

Particle size reduction and the formation of dispersions, emulsions and other delivery vehicles or matrices comprising phytosterols and using microfluidization has not heretofore been explored or achieved. Herein lies the core of the present invention. Equipment for this purpose is commercially available from Microfluidics Corporation, Newton, Mass. (USA). Microfluidization employs the forces of shear, impact and collision to achieve these ends as described in detail below.

Two important features define the microfluidization apparatus:

- i) an interaction chamber having liquid jet paths of fixed geometry; and
- ii) an intensifier pump allowing delivery of the liquid to the interaction chamber at constant pressure.



The intensifier pump may be any high-pressure pump but it is most preferred to use an air-driven or electric-driven hydraulic pump. The interaction chamber is generally a ceramic block with a system of channels running therethrough. Under high pressure, which can incrementally and accurately be increased or decreased over a wide range simply by adding or subtracting pneumatic or hydraulic pressure, phytosterols and/or phytostanols, previously dissolved, dispersed or otherwise suspended in a liquid vehicle enter the chamber and are split into two or more streams. The streams are turned at right angles and impacted upon each other resulting in shear (laminar flow), turbulence and cavitation (vapour bubble implosion). This technique exposes each volume of fluid to forces which are relatively consistent throughout the entire process thereby producing microparticles of phytosterols and/or phytostanol of substantially uniform size and shape. In a preferred form the microfluidizer is operated between 15,000 and 23,000 psi. Increasing the number of passes through the chamber further decreases the particle size.

The microparticulate phytosterol and /or phytostanols so formed may be used without further modification or adaptation and incorporated directly into foods, beverages, nutraceuticals and pharmaceuticals or, alternatively may be further treated (e.g. esterified and/or hydrogenated) and/or formed into other delivery vehicles such as emulsions, microemulsions, liposomes, hydrated lipid systems, cyclodextrin or bile acid complexes and the like prior to such incorporation.

Although it is known in the art to produce microparticles comprising various biological materials, what has not heretofore been achieved or appreciated is the formation of phytosterol and/or phytostanol microparticulates using microfluidization and the benefits afforded by this formation. US Patent No. 5,500,161 to Andrianov et al. describes a method of preparing hydrophobic polymeric microparticles suitable for encapsulating material such as proteins, liposomes and cells. One preferred means to coagulate the polymer with the material is via microfluidization. Similarly, US Patent No. 5,516,543 to Amankonan et al. discloses the preparation of oil-coated microparticulate gellan gum suitable for use as a fat replacer or extender.

Within the scope of the present invention, the vehicle into which the phytosterol and/or phytostanol component is dispersed or otherwise suspended may be any organic, inorganic or aqueous media or any food, beverage, nutraceutical or pharmaceutical matrix, including, but not limited to: all edible oils such as canola oil, soybean oil, corn oil, coconut oil, cottonseed oil, olive oil, palm oil, peanut oil, rapeseed oil, safflower oil, sesame oil and sunflower oil (vegetable oils and soybean oils being the most preferred) and the like, all fats, butter (including cocoa butter), lard, milk and other dairy beverages and all aqueous solutions, dispersions and suspensions including soy beverages, colas, juices and dietary supplement/meal replacement drinks.

## **2) Particle Size Reduction by other Shear Forces**

Although microfluidization is the most preferred method, microparticles of phytosterols may also be prepared within the scope of the present invention by using air-atomization or pneumatic nozzles or by using high shear mixers or colloid mills. Colloid mills force liquid through very small clearances (for example 1/1000 of an inch) between two opposing phases known as the rotor and the stator, thereby producing microparticles by shear energy. The preferred equipment for such shearing force is an air atomizer sold by Turbotak Corporation (Ottawa) or an ultrasonic spray nozzle such as Sonimist sold by Medsonic Inc. (Farmingdale NY).

## **Incorporation Phytosterols into Delivery Vehicles**

In a further aspect of the present invention, there is provided a method by which one or more phytosterols, phytosterols or mixtures or both may be incorporated into a suitable delivery system using microfluidization technology. A composition of the phytosterols and/or phytosterols is simultaneously introduced into the interaction chamber of a microfluidizer along with a stream comprising the delivery vehicle into

which it is desired that the phytsterol/phytostanol be incorporated. The microfluidizer is operated at the desired pressure and the resultant product is a vehicle into which microparticulates of the phytsterol/stanol have been uniformly and evenly distributed. As described above, when the particle size of the phytosterols/stanols is decreased, the efficacy and stability of delivery vehicle is enhanced. The delivery vehicle may be any organic, inorganic or aqueous media or any food, beverage, nutraceutical or pharmaceutical matrix, including, but not limited to any edible oil such as canola oil, soybean oil, corn oil, coconut oil, cottonseed oil, olive oil, palm oil, peanut oil, rapeseed oil, safflower oil, sesame oil and sunflower oil (vegetable oils and soybean oils being the most preferred); any fat-based food matrix such as milk, cream and other dairy products, lard, butter (including cocoa butter) or animal fat; or any beverage such as colas, soft drinks, juices, soy beverages, and dietary supplement/meal replacement drinks. This list is not intended in any way to be exhaustive.

Furthermore, in another embodiment of this invention, when phytosterols and/or phytostanols are incorporated into a delivery vehicle or "base matrix" using microfluidization technology, this base matrix can then further be used to prepare, in particular, other foods and beverages, or alternatively pharmaceuticals. For example, phytosterols and/or stanols may be incorporated at varying concentrations, but most preferably at concentrations up to 12%, into milk using microfluidizing technology thereby creating a stable dispersion. The milk so prepared is then a suitable base for making other products such as ice cream, cream for butter and cheeses and yoghurt and other dairy products. When the base matrix is fat like cocoa butter, the phytosterols and/or phytostanols may be incorporated therein using microfluidizing technology and subsequently used to make chocolate and other confections. When the base matrix is a fat or fat blend, for example comprising lard, lard flakes, palm oil, palm kernel oil, cottonseed oil, coconut oil, soybean oil, corn oil, rapeseed oil or the like, an emulsion is formed using the method of the present invention which subsequently can be used to prepare cereal bars. Furthermore, when the base matrix is a fat or fat blend or edible oil, the product so formed by microfluidizing with phytosterols and/or phytostanols is equally suitable for many pharmaceutical applications, including the incorporation of the

product into gel caps. The uses of microparticulate phytosterols/stanols are varied and accordingly, it is not intended that the present invention be limited to any particular base vehicle to the exclusion of others.

In addition, edible emulsions comprising phytosterols an/or phytostanols may be formed using the microfluidizing technology. For example, and as described further below, phytosterols and/or phytostanols can be emulsified into oils and fats and then subsequently used to produce dressings such as salad and vegetable dressings, mayonnaise, dairy and non-dairy spreads, chocolates and other confections and beverages.

In a preferred form, the incorporation of phytosterols and/or phytostanols into the base matrix or delivery vehicle is as follows: non-milled phytosterols and/or phytostanols in powder form, preferably of particle size around 100 um, are blended or suspended into the delivery vehicle (for example, fats, oils or aqueous solutions as described above) using a batch mixer, preferably a high shear mixer such as T50 Ultra Turrex. Subsequently, the blend is forced into a microfluidizer interaction chamber using a pump or compressed air. Microfluidization is performed under pressure of 15,000 to 23,000 psi, most preferably around 20,000 psi. Several passes through the chamber may be required in order to achieve the preferred phytosterol/stanol particle size i.e. under 20 microns, most preferably in the range of 10-20 microns.

As used herein, the term phytosterol includes all phytosterols without limitation, for example: sitosterol campesterol, stigmasterol, brassicasterol, desmosterol, chalinosterol, poriferasterol, clionasterol and all natural or synthesized forms thereof, including isomers. The term "phytostanol" includes all hydrogenated (saturated) or substantially hydrogenated phytosterols and all natural or synthesized forms thereof, including isomers. It is to be understood that modifications to the phytosterols and/or phytostanols i.e. to include side chains, also falls within the purview of this invention. It is also to be understood that this invention is not limited to microparticulates of any particular one or combination of phytosterols and/or phytostanols. In other words,

microparticulates of any phytosterol or phytostanol alone or in combination with other phytosterols and/or phytosterols in varying ratios as required may be formed in accordance with the present invention. For example, the composition referred to in US Patent Serial No. 5,770,749 to Kutney et al. (hereinafter called "Kutney et al." and incorporated herein by reference) may be formed into microparticulates or otherwise incorporated into a delivery system using a microfluidizer in accordance with the present invention.

Phytosterols and phytosterols may be procured from a variety of natural sources. For example, they may be obtained from the processing of plant oils (including aquatic plants) such as corn oil and other vegetable oils, wheat germ oil, soy extract, rice extract, rice bran, rapeseed oil, sesame oil, fish oils and other marine-animal oils. Without limiting the generality of the foregoing, phytosterols and/or phytosterols may be extracted from tall oil-derived pulping soap (a by-product of forestry practises) as described in Kutney et al.

In one embodiment of the present invention, the phytosterols and/or phytosterols are isolated from the source and formed into a solid powder through either precipitation, filtration and drying, spray drying, lyophilization or by other conventional work-up techniques. This powder form may then be incorporated into a base matrix or delivery vehicle using the microfluidizing technology as described above. In other words, this powder or alternatively, phytosterols/stanol directly from the source (e.g. vegetable oils) without any prior work-up techniques, may be either:

- 1) exposed to impact forces just to reduce the particle size of the constituent phytosterols/stanol; or
- 2) incorporated into a base matrix or delivery vehicle (e.g. milk, fat cream or the like) using microfluidizing technology, thereby not only reducing the particle size of the phytosterols/stanol but assisting in the uniform dispersion throughout the delivery vehicle; or

- 3) formed into emulsions using microfluidizing technology.

### **Emulsions**

Emulsions are finely divided or colloidal dispersions comprising two immiscible liquids or "phases", e.g. oil and water, one of which (the internal or discontinuous phase) is dispersed as droplets within the other (external or continuous phase). Thus, an oil-in-water emulsion consists of oil as the internal phase and water as the external or continuous phase, the water-in-oil emulsion being the opposite.

A wide variety of emulsified systems may be formed comprising phytosterols and/or stanols and using microfluidizing technology including standard emulsions and microemulsions.

Generally, emulsions comprise oil and water phases, emulsifiers, emulsion stabilizers, and optionally thickening agents, preservatives, colouring agents, flavouring agents, pH adjusters and buffers, chelating agents, vitamins, anti-foam agents, tonicity adjusters and anti-oxidants. Suitable emulsifiers include (wherein bracketed numerals refer to the preferred HLB value) include: anionic surfactants such as alcohol ether sulfates, alkyl sulfates (30-40), soaps (12-20) and sulfosuccinates; cationic surfactants such as quaternary ammonium compounds; zwitterionic surfactants such as alkyl betaine derivatives; amphoteric surfactants such as fatty amine sulfates, difatty amine sulfates, difatty alkyl triethanolamine derivatives (16-17); and nonionic surfactants such as the polyglycol ether derivatives of aliphatic or cycloaliphatic alcohols, saturated fatty acids and alkylphenols, water-soluble polyethyleneoxy adducts onto polypropylene glycol and alkyl polypropylene glycol, nonylphenol polyoxyethanols, castor oil polyglycol ethers, polypropylene/polyethylene oxide adducts, tributylphenoxy-polyethoxyethoxyethanol, lanolin alcohols, polyethylated (POE) alkyl phenols (12-13), POE fatty esters poloxamers (7-19), POE

glycol monoethers (13-16), polysorbates (17-19) and sorbitan esters (2-9). This list is not intended to be exhaustive as other emulsifiers are suitable.

Suitable emulsion stabilizers include, but are not limited to, lyophilic colloids such as polysaccharides, acacia, agar, alginic acid, carrageenan, guar gum, karaya gum, tragacanth, xanthan gum, amphoterics (e.g. gelatin) and synthetic or semi-synthetic polymers (e.g. carbomer resins, cellulose ethers and esters, carboxymethyl chitin, polyethylene glycol-n (ethylene oxide polymer  $H(OCH_2CH_2)_nOH$ ); finely divided solids including clays (e.g. attapulgite, bentonite, hectorite, kaolin, magnesium aluminum silicate and montmorillonite), microcrystalline cellulose oxides and hydroxides (e.g. aluminum hydroxide, magnesium hydroxide and silica); and cybotactic promoters/gellants (including amino acids, peptides, proteins, lecithin and other phospholipids and poloxamers.

Suitable anti-oxidants include: chelating agents, such as citric acid, EDTA, phenylalanine, phosphoric acid, tartaric acid and tryptophan; preferentially oxidized compounds such as ascorbic acid, sodium bisulfite and sodium sulfite; water soluble chain terminators such as thiols, and lipid soluble chain terminators such as alkyl gallates, ascorbyl palmitate, t-butyl hydroquinone, butylated hydroxyanisole, butylated hydroxytoluene, hydroquinone, nordihydroguaiaretic acid and alpha-tocopherol. Suitable preservatives, pH adjusters and buffers, chelating agents, osmotic agents, colours and flavouring agents and their uses are well known in the art and can be added to the emulsions of the present invention as required.

It is important to note that the phytosterols and/or stanols may be either dispersed or suspended in *either* the oil or fluid/semi-fluid phase depending on the ultimate delivery vehicle sought to be created. For example, in preparing a beverage, the phytosterol/stanol may be suspended in the fluid portion and subsequently microfluidized. One mode to prepare a soy beverage is described in Example 5. Alternatively, in preparing a non-dairy spread, the phytosterol/stanol may be dispersed

or suspended in a vegetable oil as described most preferably in Example 2 hereinbelow.

The preferred preparation of emulsions comprising phytosterols and/or stanols using microfluidizing technology in accordance with the present invention is as follows: the phytosterols and/or stanols are dispersed or suspended in an oil (or fluid) phase; the oil (or fluid) phase is then combined with a fluid or semi-fluid (or oil) phase along with an emulsifier, and any optional ingredients as listed above such as a thickening agent, to form a "blend"; the blend is then introduced into the microfluidizer at a pressure suitable to form and stabilize the emulsion. It is preferred that the oil phase comprises edible oils and fats, most preferably, vegetable oils. It is contemplated that many types of emulsions may be prepared using this process, including the formation of dairy and non-dairy spreads comprising one or more phytosterols and/or stanols.

In a further embodiment of the present invention, once such an emulsion is formed it may be encapsulated in a carbohydrate shell by a further pass through the microfluidizer as follows: blending the emulsion described above with a solution or suspension comprising one or more carbohydrates, preferably complex carbohydrates such as polysaccharides (for example: starch, inulin, glycogen) and/or one or more simple sugars such as glucose, fructose and the like—an appropriate suspension is corn syrup) and introducing this blend so formed into a microfluidizer at a suitable pressure. After subsequent spray drying, the resultant product is a core of phytosterol and fat or oil encapsulated in an outer carbohydrate shell.

## EXAMPLES

The following examples are intended merely to be illustrative and not limiting as to the scope of the present invention.



**Example 1: Preparation of yoghurt comprising microparticulates of phytosterols and/or phytostanols**

A composition of plant sterols/stanols having campesterol (14.5%), campestanol (2.4%), beta-sitosterol (50.9%) and sitostanol (18.9%) (hereinafter referred to as "Phytrol™") was mixed with non-fat milk powder in the ratio of 1:7 to 1:8. About 6 L of milk mix was prepared from whole milk, skimmed milk and the Phytrol containing milk powder. Milk was standardized to 0.75-1% fat, 12-13% solids and 0.5-1% Phytrol using the Pearson's Square method (Hyde, KA and Rothwell, J. 1973, In Ice Cream, Churchill Livingstone Ltd., London U.K.). The milk mix was permitted to remain at room temperature for 30 minutes to re-hydrate the milk powder and then it was homogenized using a high-speed microfluidizer commercially available from Microfluidics Corporation, Newton, Mass. (USA). Next, milk was then pasteurized at 69°C (156°F) for 30 minutes (batch/vat), cooled to 44° C and held at this temperature for up to 30 minutes.

About 3% by weight of active yoghurt culture containing *Lactobacillus bulgaricus* and *Streptococcus thermophilus* in the ratio of 1:1 were carefully introduced into the warm milk mix. After gentle mixing, the inoculated milk was distributed into 125G containers filling to near top. The containers were thermally sealed with aluminum leads and placed in an incubator (44°C) equipped with a good uniform air circulator and temperature controller. Filled containers were permitted to remain at 44°C for 3-5 hours, until a firm, smooth gel was formed. During incubation, pH was monitored periodically. When pH reached about 4.5, the yoghurt was withdrawn from the incubator, chilled quickly and stored at 4°C.

**Example 2: Preparation of a Vegetable Spread/Emulsion comprising microparticulates of phytosterols and/or phytostanols**

A mixture of soybean oil and palm oil with Phytrol in the concentration range of 50-80% can be used to develop an emulsion. A small portion of hydrogenated vegetable oil (2-5%) can be added in order to obtain the desired texture. Two types of emulsions are

possible: oil-in-water, which is preferable for the development of the low-fat spread and water-in-oil, which is preferable for some other applications. Appropriate emulsifiers or stabilizing agents such as lecithin, polysorbates and lactylates are used to stabilize the emulsion. Thickening agents such as gums (xanthan gum, locust bean gum, guar gum etc.), gelatin, pectins, and agar may also be added. To colour the spread, beta-carotene, caramel colour and FD&C yellow dye may be used. Furthermore, enriching the oil phase with vitamins A and D as well as with essential polyunsaturated fatty acids is possible.

A spread composition is as follows:

Vegetable oil (liquid)	50-80%
Vegetable, saturated fat	0-5%
Phytrol	9-15%
Emulsifier	0.2-1%
Thickening agent	0-10%
Butter Flavour, colourant, salt	various, as required
Water	to 100%

All of the ingredients are blended in a stainless steel vessel equipped with a high sheer batch mixer such as the T50 Ultra Turrex. After blending is completed, and the mix has the consistency of heavy cream, the blend is tempered to a consistency of margarine by letting it sit for a couple of hours. To stabilize the emulsion and concomittantly to reduce the particle size of the phytrol component, the spread is homogenized in a microfluidizer.

**Example 3: Preparation of a Cereal Bar comprising microparticulates of phytosterols and/or phytostanols**

It has been found by the applicants herein that Phytrol can be dispersed in fat up to 27% (and possibly more). For this reason, cereal bars having fat-based binders have been

investigated. In this example, Phytrol is dispersed in fat to form a continuous emulsion. This fat component is then combined with carbohydrates and optionally with other ingredients to form a binder suitable to maintain the strength and elastic properties of the cereal bar.

**a) Binder**

Generally, the fat-binder composition in cereal bars ranges from about 20-85% fat, and 20-60% carbohydrates by weight. The strength of the cereal bar is improved with the addition of up to 1% monoglycerides and diglycerides, however, since they have relatively high melting points compared to triglycerides, they should be used only in small proportions. Optionally, various emulsifiers, film formers (e.g. sodium caseinate or alternatively egg albumin, soy protein), colour and flavour components, vitamins and minerals may be added.

**A binder composition is as follows:**

Phytrol containing fat	40%
Sucrose	22%
Water	28%
Sodium Caseinate	5%
Lecithin	2%
Glycerin	3%

These ingredients are mixed at room temperature or added to boiled sucrose in water. Mixing is carried out vigorously using a suitable mixer (e.g. Hobart mixer) with the aim being to disperse the fat globules (discontinuous phase) in the film former/sucrose syrup (continuous phase). During this mixing process, fat is encapsulated. To determine whether this process is complete, place one drop of the dispersion in water at 60°C. If fat is released, mixing is not complete and should be continued.

**a) cereal bar**

Any combination of oats, crisp cereals (corn and wheat flakes, Rice Krispies™), nuts, raisins and fruits, in various proportions comprise the "edible particles". All edible particles should be ready-to-eat. Cereals can be extruded, toasted or roasted in unsaturated oil such as soy or canola oil.

**Composition of cereal bar**

Binder (with Phytol)	40%
Edible particles	55%
Water	5%

**Edible Particles:**

Rolled oats	40%
Crisped rice	15%
Puffed barley	15%
Dried Apple Dices	15%
Shredded Coconut	7.5%
Raisins	7.5%

All of these ingredients are mixed thoroughly in a Hobart Mixer equipped with a kneeling device and a rotating bowl. The binder may be heated up to 40-50°C and placed first in the bowl followed by the other ingredients. Thorough mixing without causing size reduction of the edible particles should be used the criterion to set up time of mixing. After mixing is complete, mixed material is placed in a forming mold (10x50x0.6 cm) and pressed with a roller. After removal from the mold, it is cut into 4x10 cm ready-to-eat cereal bars. After forming and cutting, the bars may be single or double enrobed using dairy-based or chocolate cover. Bars should be stabilized at 10°C for 15-20 minutes before packing.

**Example 4: Preparation of Chocolate Confection comprising microparticulates of phytosterols and/or phytostanols**

Chocolate is a dispersion of sugar and cocoa particles in a continuous phase of cocoa butter. The solid particles should generally be less than 20  $\mu\text{m}$  in diameter for the chocolate to have a smooth texture.

To make Phytrol-containing chocolate, Phytrol can either be mixed with cocoa particles (having undergone some impact procedure as described herein in order to reduce particle size) and used as such or alternatively Phytrol can be incorporated into cocoa butter using microfluidizing technology. Plain, white or milk chocolate can be made.

In the first approach, microparticulate Phytrol is mixed with cocoa powder, sugar, milk powder, emulsifier (soy lecithin), a film former and flavour agents (e.g. natural or artificial vanillin flavour). The dry mixing is conducted using a batch mixer such as T50 Ultra Turrex. Subsequently, cocoa butter and milk are added and the formulation mixed thoroughly. After mixing, chocolate mass is tempered and used for molding.

In the second approach, Phytrol is incorporated directly into the cocoa butter. Cocoa butter is mixed with non-milled Phytrol powder and then passed through a microfluidizer (M-110Y Microfluidics International Co., Newton, Mass. USA) until the particle size is in the range of 10-20 microns using the procedure described in Example 2.

Once Phytrol-containing Butter is produced it is then used to prepare chocolate.

#### **Example 5: Preparation of Soy Drink comprising microparticulates of phytosterols and/or phytostanols**

Soy drink is made of whole soybeans with filtered or purified water. It may contain added calcium, vitamin D, vitamin B-12 and natural or artificial flavour. In this example, soy drinks are enriched with Phytrol.

Phytol is mixed with the soy drink of choice in the concentration ranges of 0.5-6% using a batch mixer (T50 Ultra Turrex). Samples are then submitted to the microfluidizer and emulsified.

**We Claim:**

1.A method of preparing microparticles of one or more phytosterols, phytostanols or mixtures of both which comprises:

- a) dispersing or suspending the phytosterols or phytostanols or mixtures of both in a semi-fluid, fluid or viscous vehicle; and
- b) exposing the vehicle so formed to impact forces.

2. The method of claim 1 wherein the vehicle is any organic, inorganic or aqueous media.

3. The method of claim 1 wherein the vehicle is a food, beverage or nutraceutical matrix selected from the group consisting of edible oils, fats, milk, creams, and aqueous solutions and suspensions.

4.The method of claim 1 wherein the phytosterols are selected from the group consisting of sitosterol, campesterol, stigmasterol, brassicasterol, desmosterol, chalinosterol, poriferasterol, clionasterol and all natural or synthesized or isomeric or saturated forms and all derviations thereof.

5.The method of claim 1 wherein the impact force is created using a microfluidizer.

6. The method of claim 1 wherein the impact force is created by an air atomization nozzle.

7. The method of claim 1 wherein the impact force is created by a pneumatic nozzle.

8. A method of incorporating one or more phytosterols; phytostanols or mixtures of both into a delivery vehicle which comprises:

- a) simultaneously introducing a solution of the phytosterols and/or phytostanols and the desired delivery vehicle into a microfluidizer; and
- b) operating the microfluidizer at a suitable pressure.

9. The method of claim 8 wherein the delivery vehicle is selected from the group consisting of all edible oils, fats, milk, creams and all inorganic or organic aqueous solutions or suspensions.

10. The method of claim 8 wherein the delivery vehicle is a vegetable oil.

11. The method of claim 8 wherein the delivery vehicle is a fat.

12. The method of claim 8 wherein the delivery vehicle is cocoa butter.

13. A method of preparing an emulsion comprising one or more phytosterols, phytostanols or mixtures of both which comprises:

- a) dispersing or suspending the phytosterols or phytostanols or mixtures of both in an oil phase;
- b) combining the oil phase so formed and a suitable semi-fluid or fluid phase to form a blend;
- c) introducing the blend into a microfluidizer; and
- d) operating the microfluidizer under suitable pressure.

14. The method of claim 13 wherein the oil phase is selected from the group consisting of one or more edible oils and fats.

15. The method of claim 13 wherein the oil phase is vegetable oil.



16. The method of claim 13 wherein the semi-fluid or fluid phase comprises any organic, inorganic or aqueous media.
17. The method of claim 13 additionally comprising the steps of blending the emulsion so formed with a carbohydrate solution to form a second blend and introducing this second blend into a microfluidizer under suitable pressure.
18. A composition comprising microparticles of one or more phytosterols, phytostanols or mixtures of both.
19. The composition of claim 18 wherein substantially all of the microparticles are less than 20 microns.
20. The composition of claim 18 additionally comprising a delivery vehicle selected from the group consisting of all edible oils, fats, milk, creams and all inorganic or organic aqueous solutions, dispersion and suspensions.
21. An emulsion comprising microparticles of one or more phytosterols, phytostanols or mixtures of both.
22. A dispersion comprising microparticles of one or more phytosterols, phytostanols or mixtures of both.
23. Fat-based comestibles comprising microparticles of one or more phytosterols, phytostanols or mixtures of both.
24. Cereal-based comestibles comprising microparticles of one or more phytosterols, phytostanols or mixtures of both.
25. Dairy-based comestibles comprising microparticles of one or more phytosterols, phytostanols or mixtures of both.

26. Chocolate confection comprising microparticles of one or more phytosterols, phytostanols or mixtures of both.

# INTERNATIONAL SEARCH REPORT

Inter. Natl Application No  
PCT/CA 00/00096

**A. CLASSIFICATION OF SUBJECT MATTER**  
IPC 7 A23L1/30 A61K9/10

According to International Patent Classification (IPC) or to both national classification and IPC

**B. FIELDS SEARCHED**

Minimum documentation searched (classification system followed by classification symbols)  
IPC 7 A23L A61K

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

**C. DOCUMENTS CONSIDERED TO BE RELEVANT**

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	WO 98 13023 A (KLASI LEENA ;TIAINEN ILKKA (FI); NURMI JUHA (FI); SUOMEN SOKERI OY) 2 April 1998 (1998-04-02) page 3, line 26 -page 4, line 30 page 5, line 12 -page 9, line 6 page 12, line 10 - line 16 examples 20-23	1-4, 18-23, 25,26
X	US 4 195 084 A (ONG JOHN T H) 25 March 1980 (1980-03-25) cited in the application column 2, line 43 - line 59 column 5, line 63 -column 6, line 6 example 1	1-5,8,9, 18,20,22
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☒ Further documents are listed in the continuation of box C.

☒ Patent family members are listed in annex.

\* Special categories of cited documents :

- \*A\* document defining the general state of the art which is not considered to be of particular relevance
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- \*L\* document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- \*O\* document referring to an oral disclosure, use, exhibition or other means
- \*P\* document published prior to the international filing date but later than the priority date claimed

- \*T\* later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
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- \*Y\* document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.
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# INTERNATIONAL SEARCH REPORT

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## C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

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X	GB 934 686 A (BOEHRINGER) 21 August 1963 (1963-08-21) page 2, line 10 - line 24	18-20,22
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